



# Investigation of the Flow Field inside a Drainage System: Gully – Pipe - Manhole

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# Introduction



One of the busiest city in Dhaka, due to 46mm of rainfall in one and a half hour; on afternoon of September 1, 2015.  
*Photo Credit: The Daily Star on September 2, 2015.*



Pluvial flooding at City centre of Coimbra on May 2006  
*Photo Source: <http://www.raingain.eu/en/actualite/flood-solutions-north-south-europe>*



Chertsey, UK on February 11, 2014  
*Photo source: The Guardian on 11 February, 2014*

# Introduction



- Flooding is one the of biggest threats for a busy urban city
- The urban drainage system is responsible for safe routing of flood water; hence an efficient drainage is mandatory
- Drainage system efficiency is dependent on the individual efficiency of each element
- Gully and Manhole are two common element of an urban drainage system
- Flow analysis inside these structures can lead to a better understanding of the efficiency of a drainage system

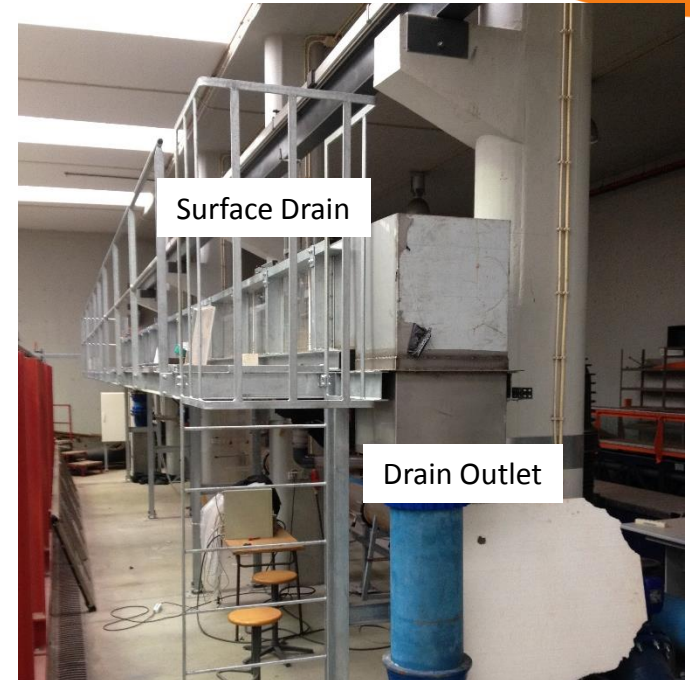
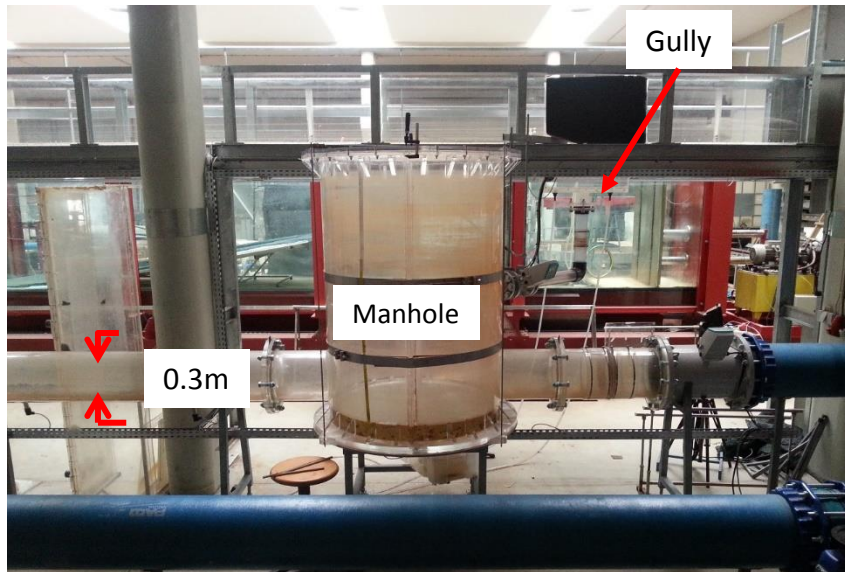
# Objective



- To validate CFD model with experimental measurement at the laboratory
- To analyse the different flow behaviour inside a gully-manhole drainage system

# Methodology

## Physical Model set up

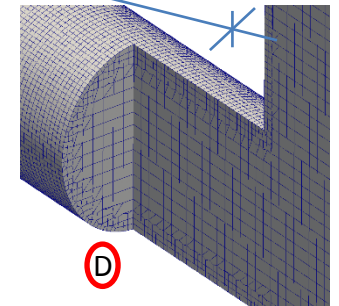
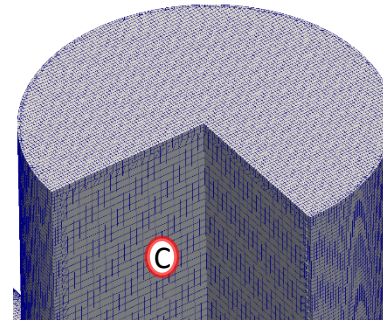
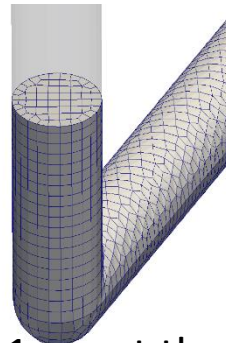
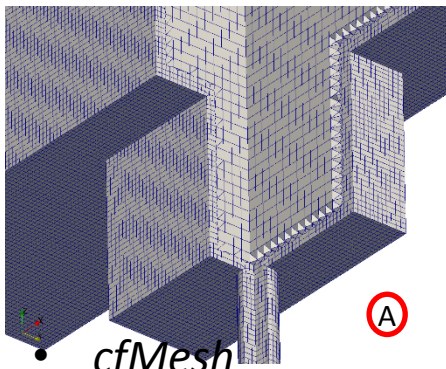
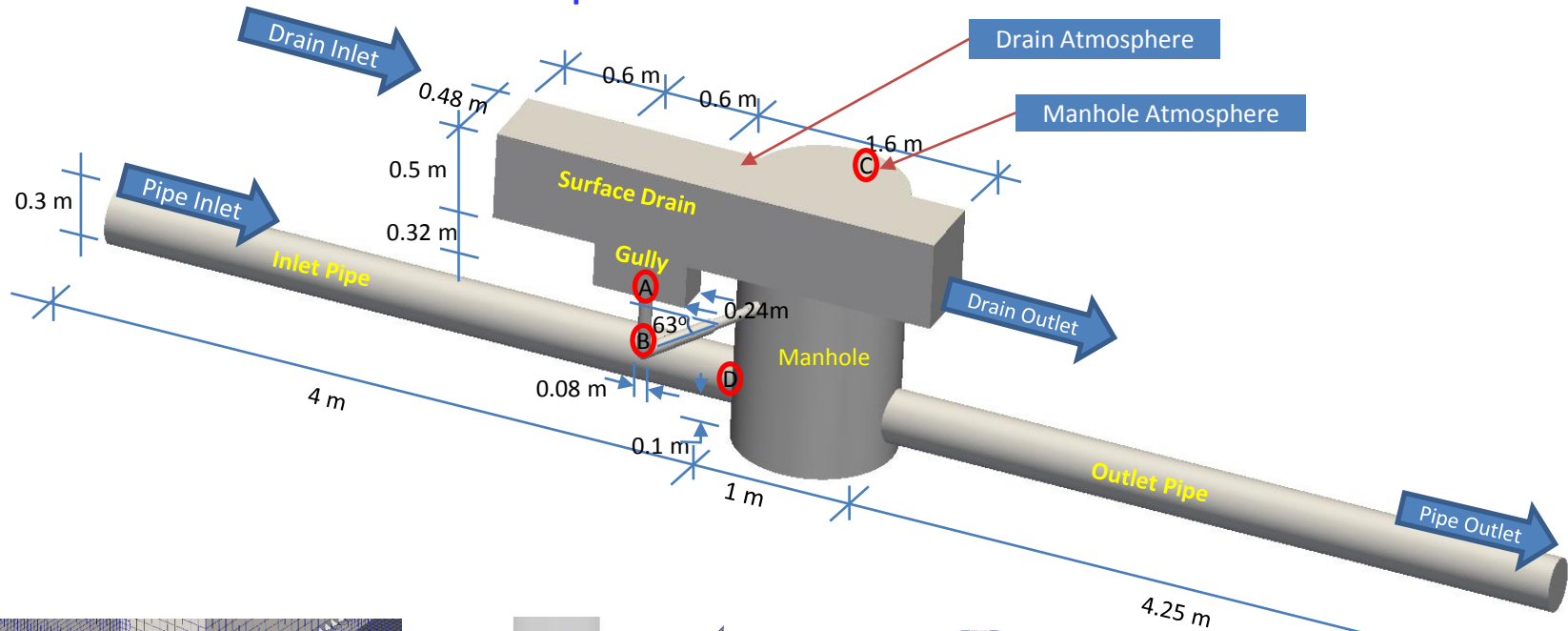


The physical model facility is installed at the Department of Civil Engineering, University of Coimbra.

- 1m diameter manholes
- Connected by a  $\varnothing 300$  sewer pipe
- 0.5m wide and 1% slopped surface
- channel
- $0.6 \times 0.24 \times 0.32$  [m] (L  $\times$  W  $\times$  D)
- gully

# Methodology

## Numerical Model set up



- cfMesh
- Mesh size 2cm

- 1 cm at the boundaries
- 821,500 computational with 1.01 million nodes

# Field Data collection



St Pedro  
Location of hydrologic data collection



# Methodology



## OpenFOAM simulation

- OpenFOAM v. 2.3.0
- *interFOAM* solver: considering isothermal, incompressible and immiscible two-phase flow (air and water for this case)
- Mass and Momentum conservation

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0$$

$$\frac{\partial \rho \mathbf{u}}{\partial t} + \nabla \cdot (\rho \mathbf{u} \mathbf{u}) = -\nabla p^* + \nabla \cdot \boldsymbol{\tau} + \mathbf{g} \cdot \mathbf{x} \nabla \rho + \mathbf{f}_\sigma$$

- Uses Volume of Fluid (VOF) method (Hirt and Nichols 1981) to track the free surface or interface location
- RAS k- $\epsilon$  turbulent model was used
- PISO algorithm is used



# Methodology



## Tests performed

- Numerical model: combination of two different experimental studies:
  1. only the manhole with inlet and outlet pipe were used; a flow of 43.7 l/s was applied through the manhole inlet.
  2. flow through the drain and gully was observed; 19.8 l/s flow was measured at the upstream of the drain inlet
- Two different Numerical simulations are tested

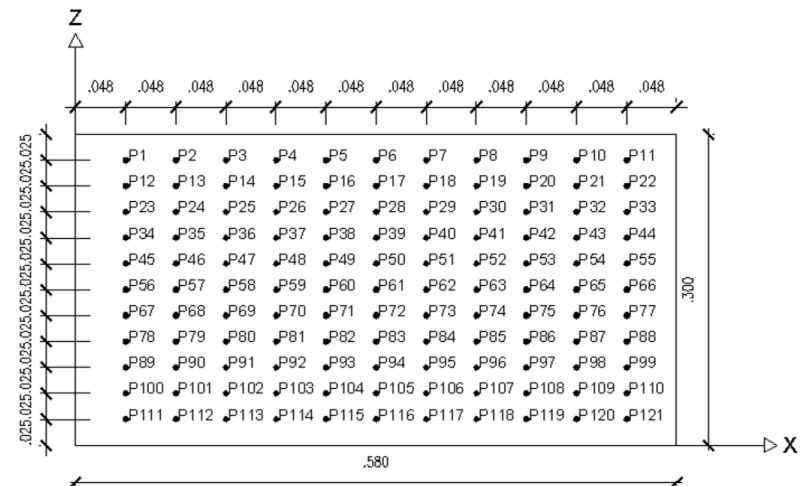
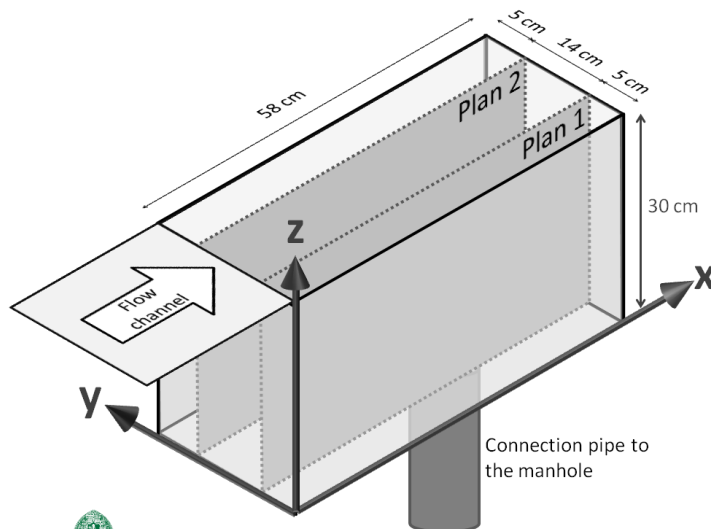
	Drain inlet Q (l/s)	Manhole inlet Q (l/s)	Manhole surcharge level (m)	Remarks
Simulation 1	19.8	43.7	0.67	Experimental case scenario
Simulation 2	19.8	43.7	1.29	Additional scenario

- 40seconds of run to reach steady state condition
- Each steady state simulation took 138hrs using 16 processors

# Results

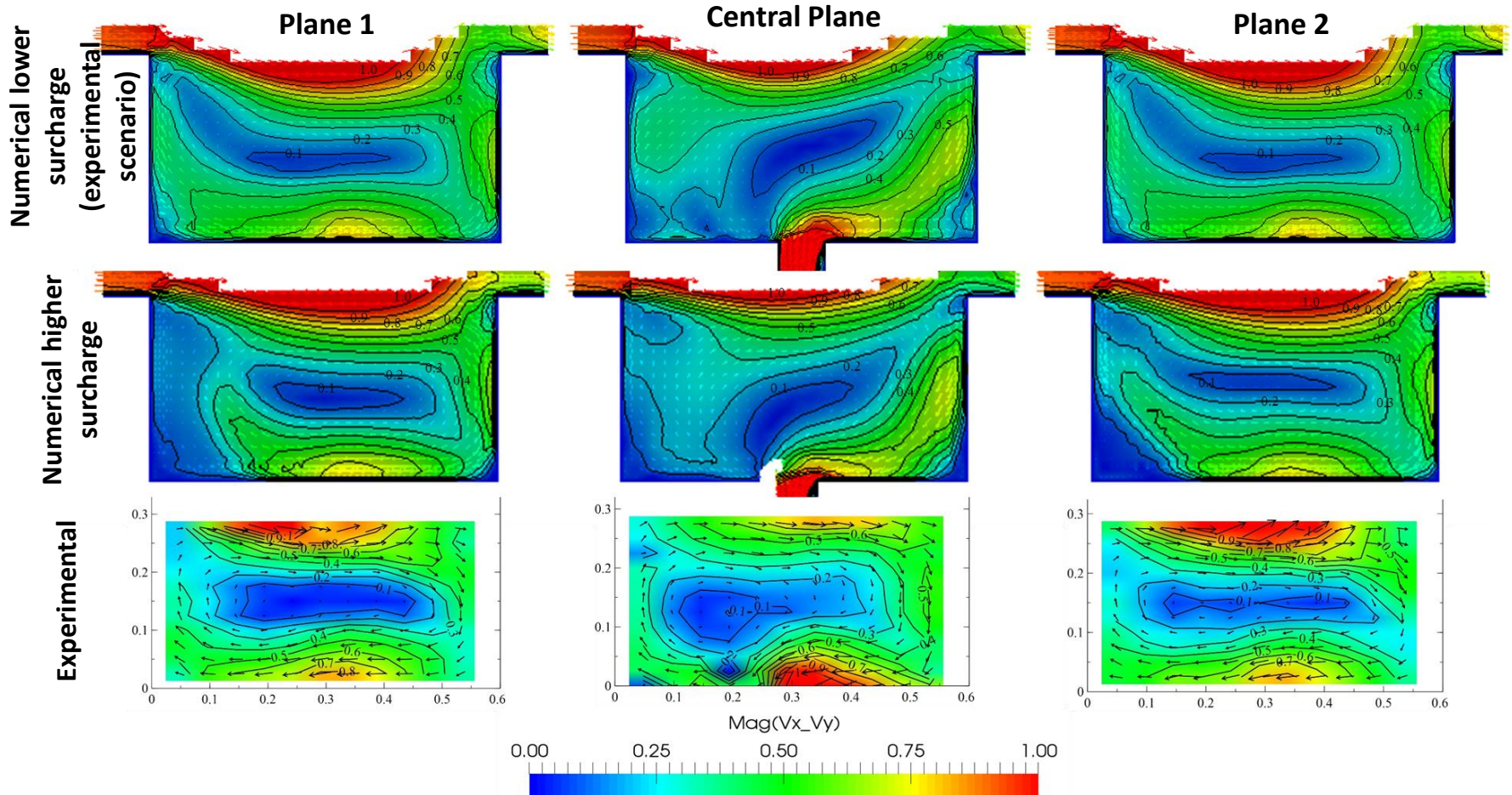
## Comparison with experimental tests performed

- During the experimental study, velocity at the gully was observed at three plane using Nortec Vectrino acoustic velocimeter
- The first and the third plane are at 5 cm distance from the longitudinal walls of the gully
- The second plane is the central plane
- Each plane contained 121 velocity measurements



# Results

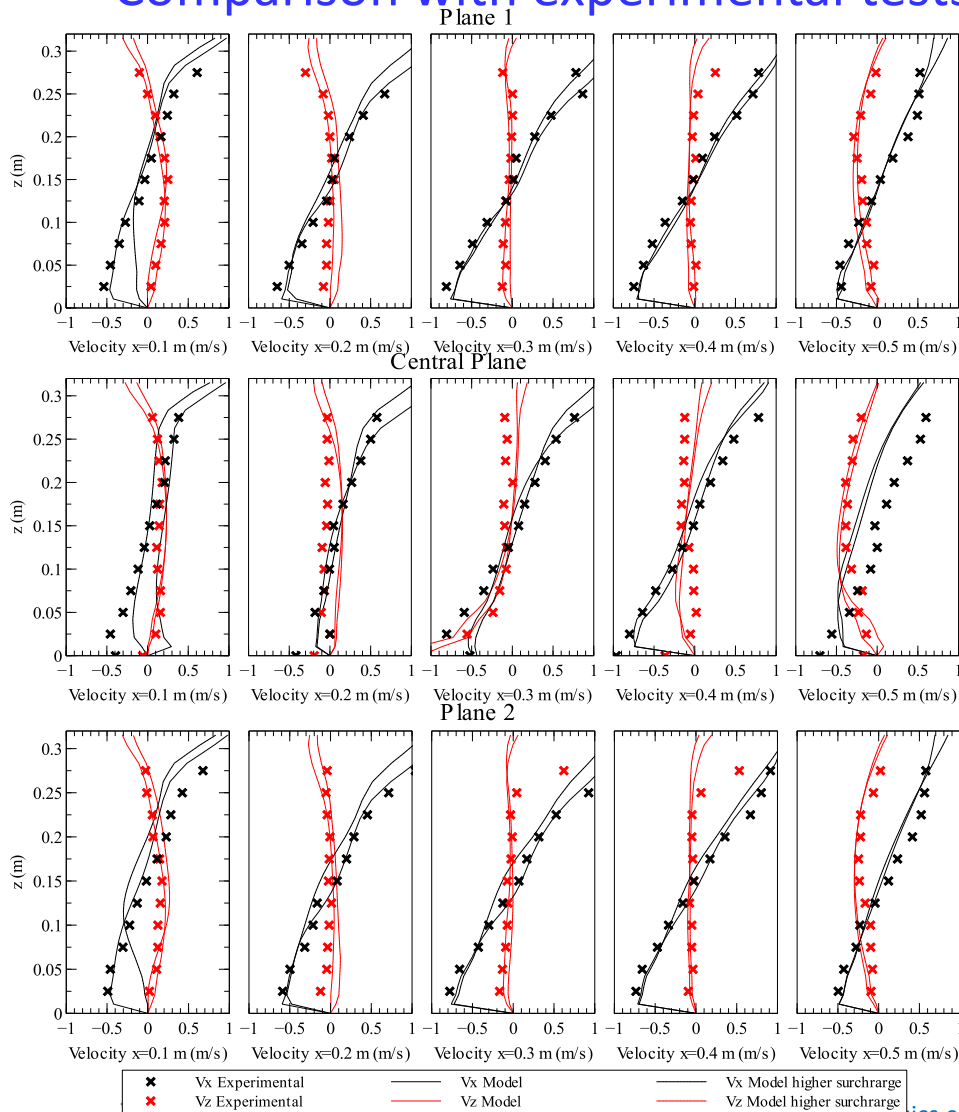
Comparison with experimental tests performed



# Results



## Comparison with experimental tests performed



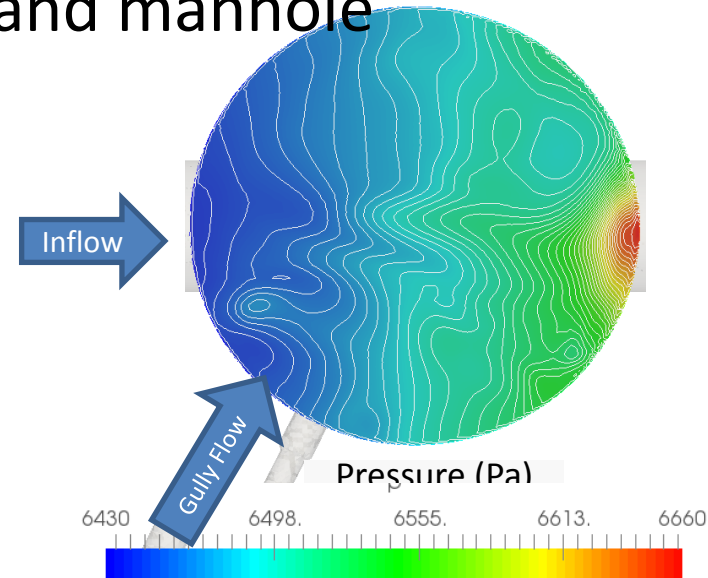
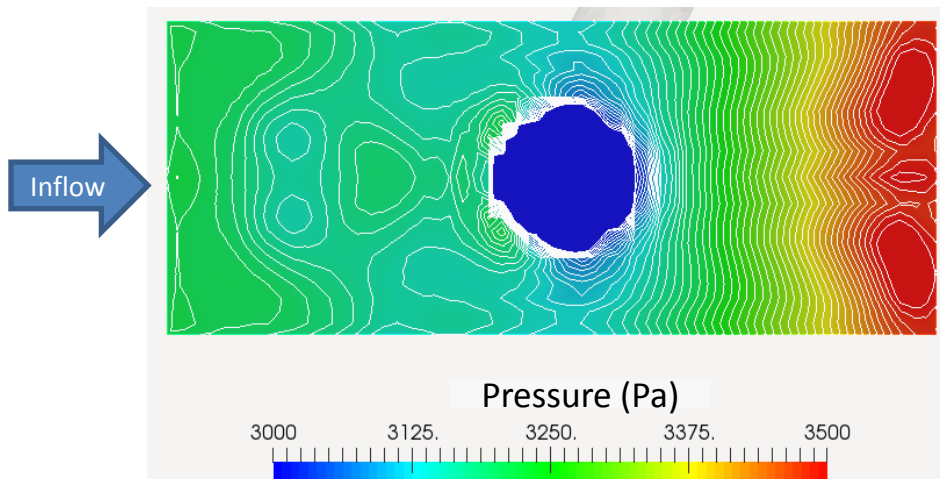
		BIAS					
		X=0.1m	X=0.2m	X=0.3m	X=0.4m	X=0.5m	Avg.
P 1	Vx	0.060	0.014	-0.078	-0.068	-0.007	<b>-0.016</b>
P C		-0.223	-0.034	-0.024	-0.009	<b>0.186</b>	<b>-0.021</b>
P 2		0.096	0.023	-0.010	-0.016	0.028	<b>0.024</b>
Avg.		-0.023	0.001	-0.037	-0.031	0.069	<b>-0.004</b>
P 1	Vz	0.004	-0.031	0.009	0.072	0.073	<b>0.025</b>
P C		-0.020	<b>-0.141</b>	0.015	-0.020	0.021	<b>-0.029</b>
P 2		-0.029	-0.021	0.069	0.079	0.089	<b>0.037</b>
Avg.		<b>-0.015</b>	<b>-0.064</b>	<b>0.031</b>	<b>0.044</b>	<b>0.061</b>	<b>0.011</b>

		r					
		X=0.1m	X=0.2m	X=0.3m	X=0.4m	X=0.5m	Avg.
P 1	Vx	0.993	0.985	0.988	0.996	0.981	<b>0.988</b>
P C		0.817	0.964	0.974	0.998	0.931	<b>0.937</b>
P 2		0.994	0.993	0.996	0.992	0.985	<b>0.992</b>
Avg.		0.935	0.981	0.986	0.995	0.966	<b>0.972</b>
P 1	Vz	0.932	0.834	0.728	0.891	0.845	<b>0.846</b>
P C		0.600	<b>-0.221</b>	0.917	<b>-0.731</b>	0.806	<b>0.274</b>
P 2		0.920	<b>0.233</b>	<b>0.129</b>	0.845	0.840	<b>0.593</b>
Avg.		<b>0.817</b>	<b>0.282</b>	<b>0.591</b>	<b>0.335</b>	<b>0.830</b>	<b>0.571</b>

# Results

## Pressure at the bottom

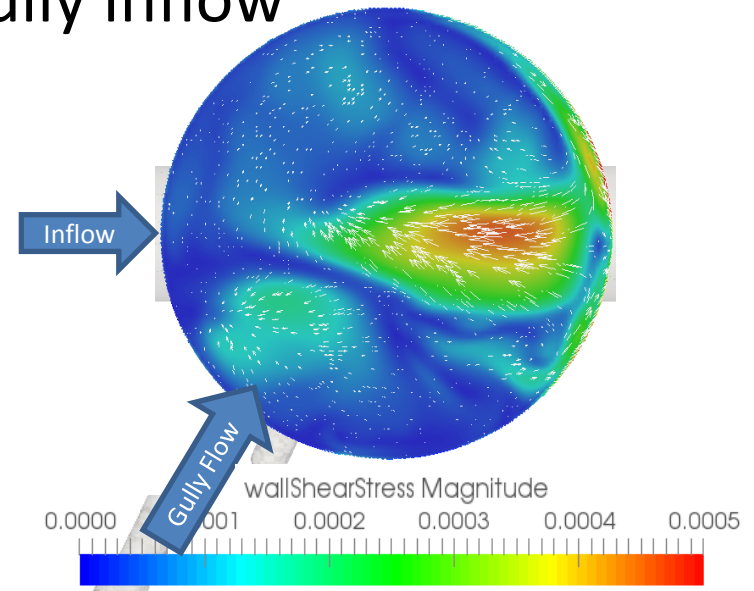
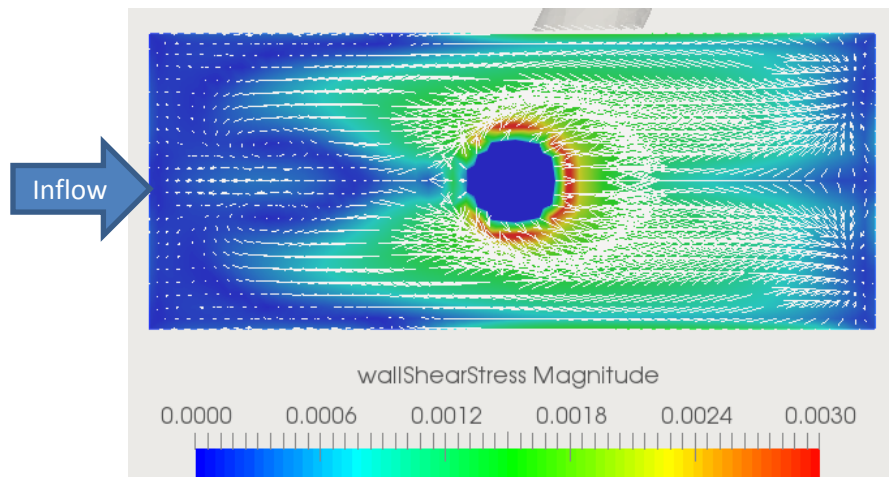
- The pressure at both the gully and manhole bottom are not uniform
- Higher pressure near the drain outlet and lower pressure at the inlet
- Difference between the max and min pressure is in the range of 300Pa and 200Pa at gully and manhole bottom respectively



# Results

## Wall shear stress at the bottom

- Like pressure map, the wall shear stress is not uniform
- The shear stress direction is opposite to the flow
- For gully, higher shear stress near the gully outlet
- For manhole, higher shear stress near the central axis
- The shear stress pattern is asymmetric for the manhole bottom, probably a result of gully inflow

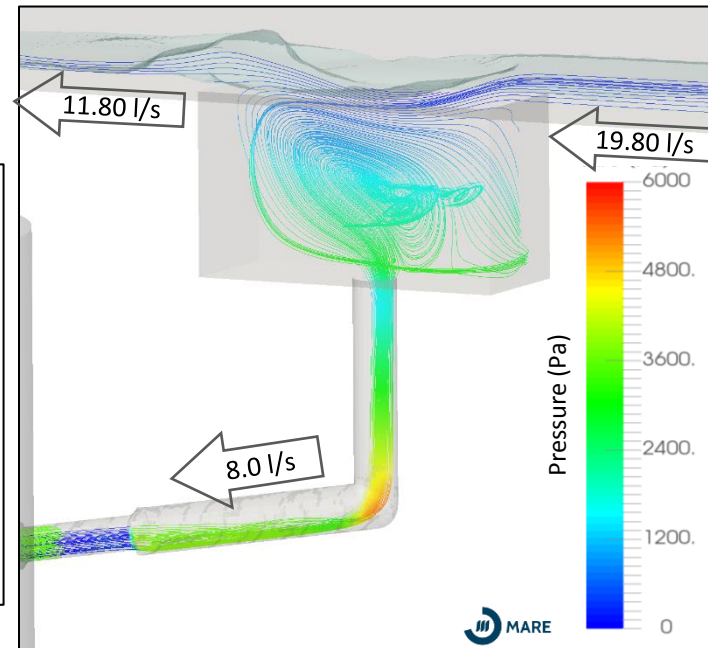
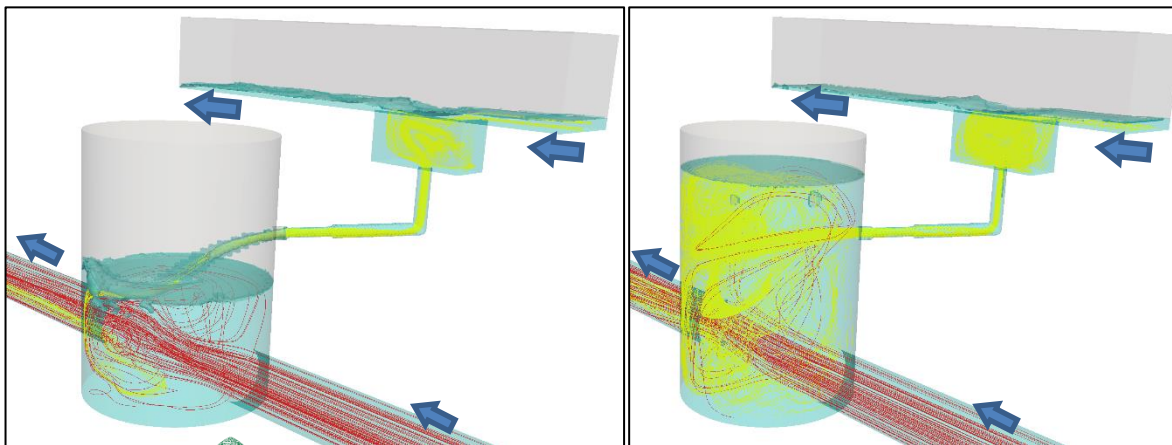


# Results

## Streamline

- Flows coming from gully and manhole inlet becomes well mixed inside manhole
- Surcharge level has influence in the vortex formation
- Fraction of the flow from drain inlet goes inside the gully and later comes out to the drain
- The gully outlet flow occupies partial area of the pipe

Flow distribution	Drain Inlet	Drain Outlet	Gully Pipe	Manhole Pipe Inlet	Manhole Pipe Outlet
Flow (l/s)	19.80	11.80	8.0	43.70	51.70



# Conclusion



- The work presented shows the first step numerical assessment of flow behaviour inside a gully-manhole drainage system
- OpenFOAM<sup>®</sup> v. 2.3.0 with solver interFOAM was used with RANS k- $\epsilon$  turbulence model
- Numerical model shows good agreement with measured velocity at the gully
- Flow streamline show different characteristics with change in surcharge level in the manhole.



# Future Work



- The model will be validated with flow measurement inside the manhole
- The work will be further developed to better understand the particulate transport phenomena inside the drainage system



**Thank you  
for your attention**

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