



# 14<sup>th</sup> IWA/IAHR International Conference on Urban Drainage

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## Comparison of manhole hydraulics using PIV and different RANS model

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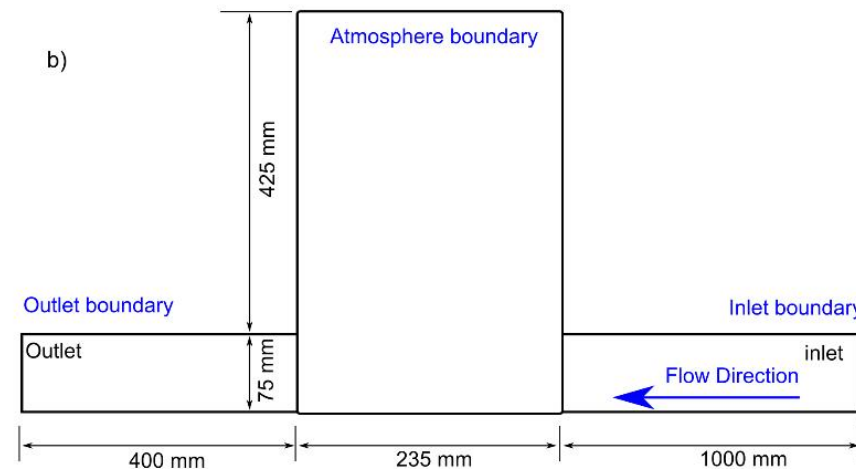
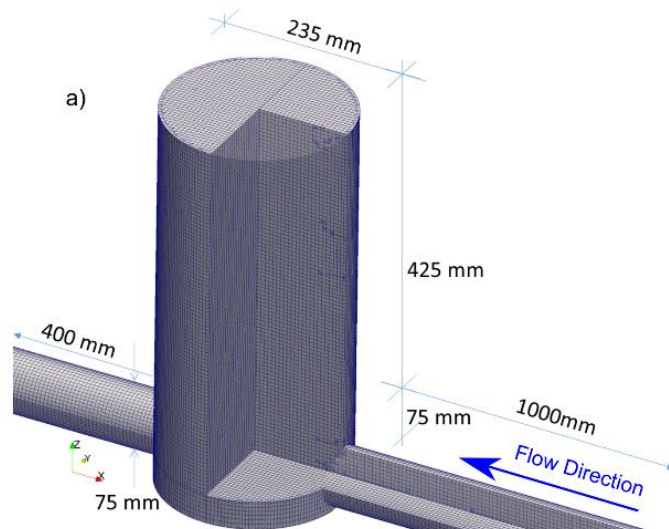
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# Introduction

- Flows in manholes are complex and may include **retardation**, **acceleration** and **rotation**
- How these complex 3D flow patterns could affect flow quantity and quality in the wider network is as yet unknown
- A **CFD model** in OpenFOAM<sup>®</sup> using four different Reynolds Averaged Navier Stokes (RANS) turbulence modelling is constructed to represent flows in the manhole
- A **2D3C stereo Particle Image Velocimetry** (PIV) measurements are made for the first time in a surcharged scaled circular manhole
- Using Laser light sheet to illuminate a 2D plane in the manhole and two cameras simultaneously to record the flow field from two different angles.
- Velocity profiles from CFD are compared with PIV data

# Numerical Model

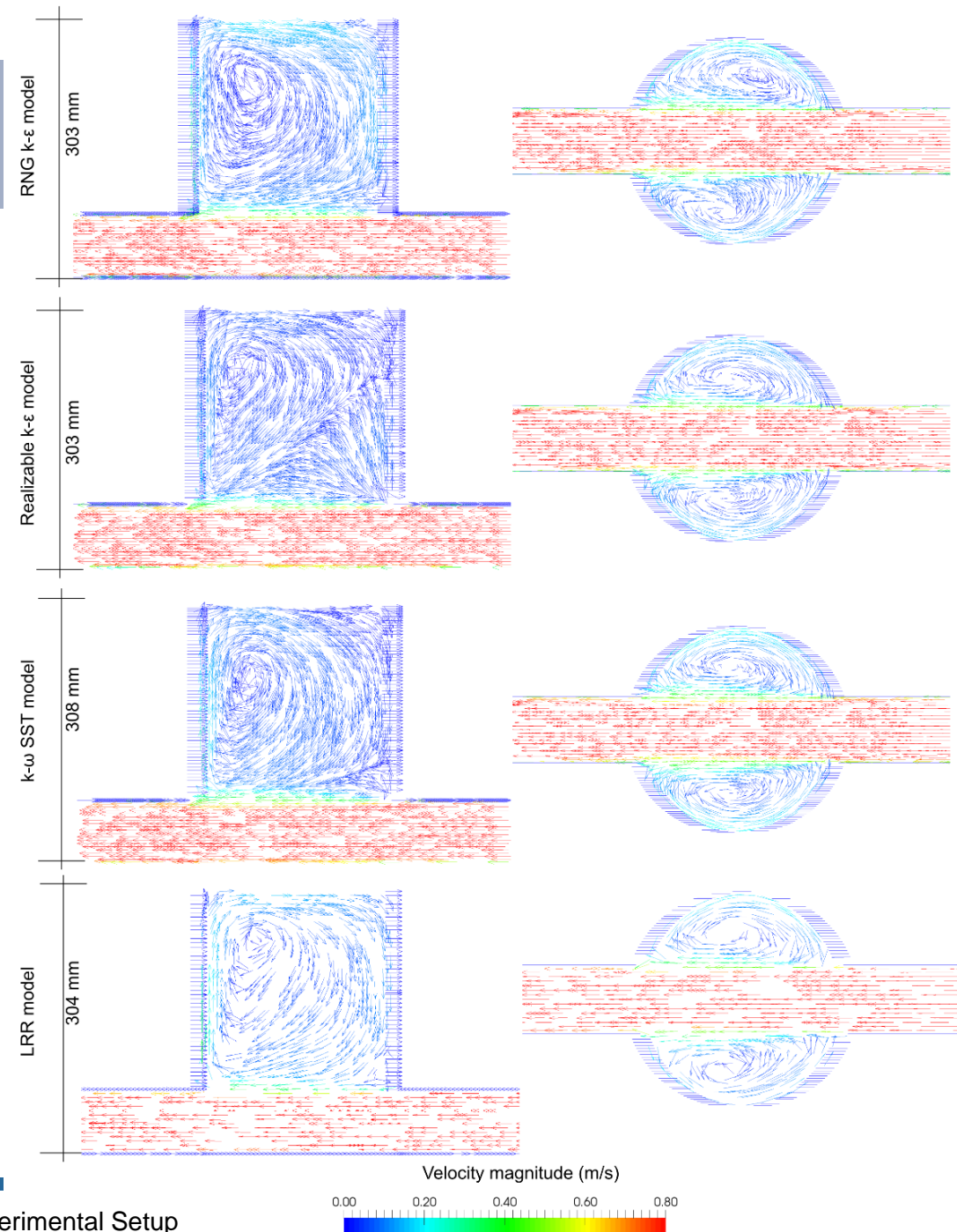
- Open source CFD model tool OpenFOAM®v4.1, with **VOF based solver interFoam**
- Cartesian mesh using **cfMesh**
- interior and the boundary mesh sizes were kept as 4 mm and 1 mm respectively
- One particular manhole flow condition was chosen:  **$Q = 3.98 \text{ l/s}$**  and the **water depth = 310 mm**.
- Fixed velocity inlet
- Fixed pressure outlet
- No wall roughness
- **noSlip** condition at wall
- $y+$  value around 5



- Four turbulence models:
1. RNG  $k-\epsilon$ ,
  2. Realizable  $k-\epsilon$ ,
  3.  $k-\omega$  SST and
  4. Launder-Reece-Rodi (LRR)

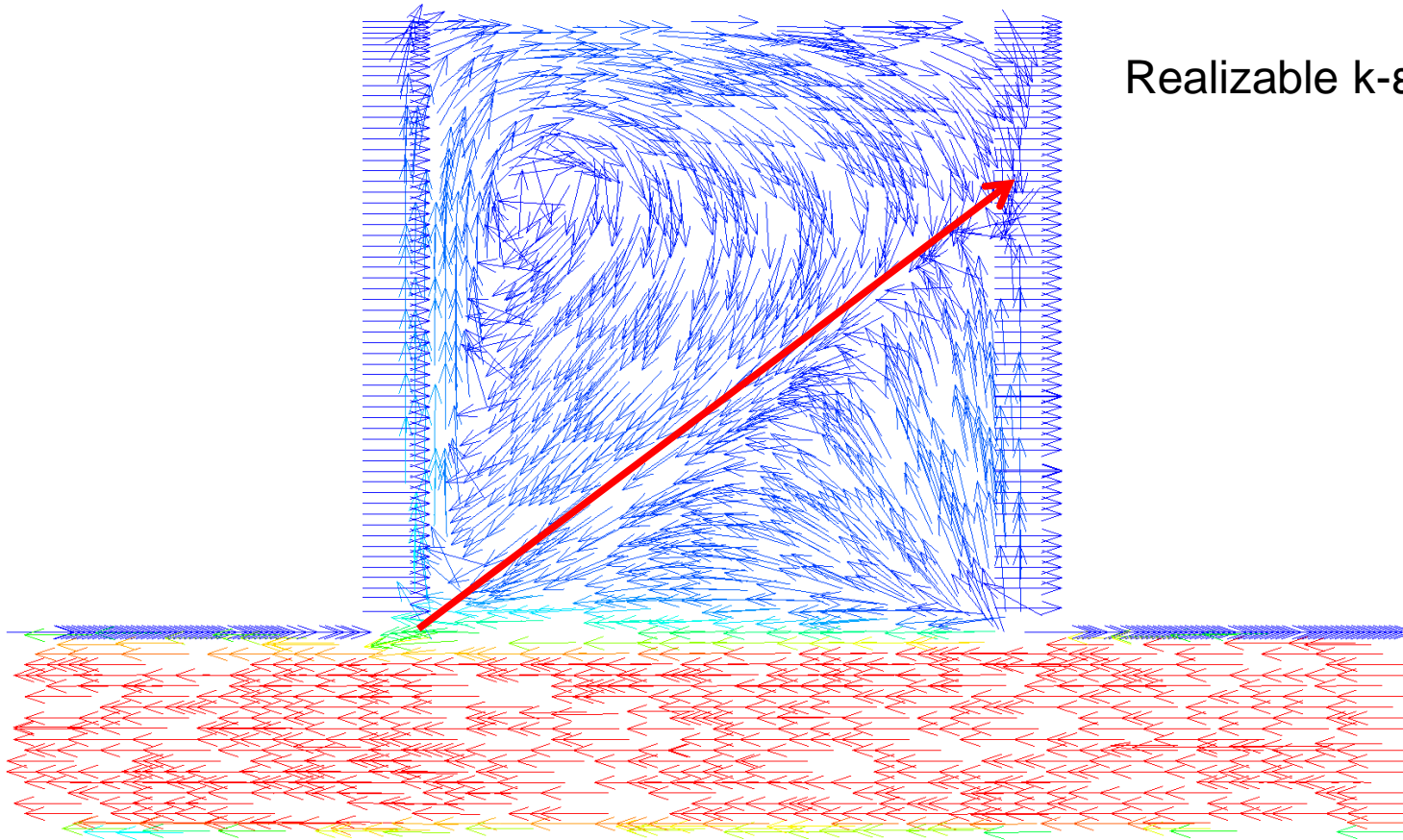
# Comparison between models

- Velocity of central vertical and the horizontal planes through the pipe axis
- Two velocity zones: **high velocity near the inlet-outlet** pipe axis due to jet and **low velocity due to recirculation**
- The **jet flow is similar** at all the four models
- The **recirculation zone is different**
- Vertical plane velocity shows different size and locations of the vertical vortex
- **Realizable k- $\epsilon$  creates a separation zone** in the middle of the manhole and pushes the vertical vortex more towards the outlet wall
- Results do not show much variation in the vortex locations at horizontal sections

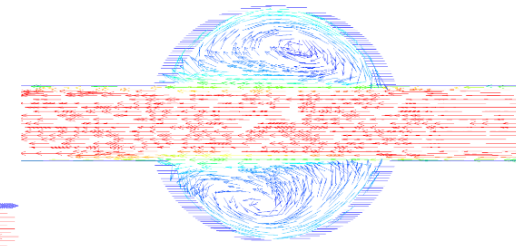
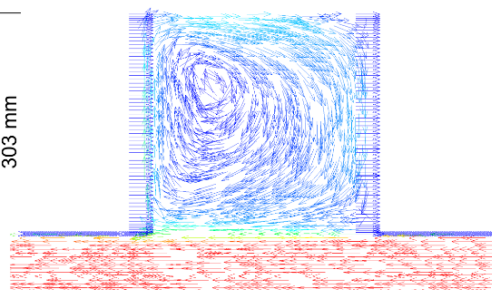


# Comparison between models

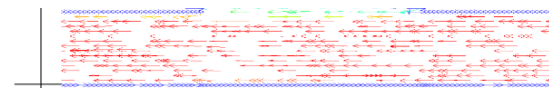
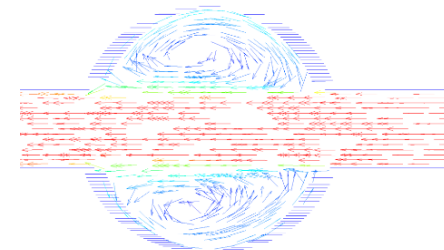
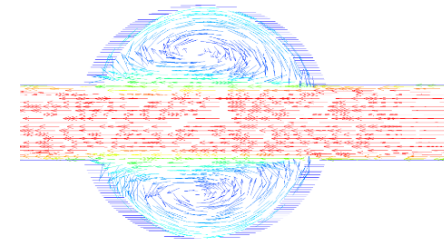
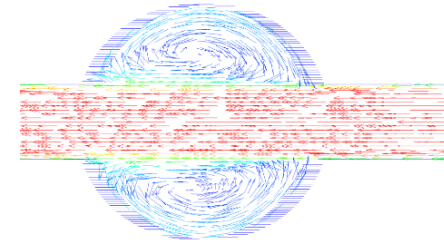
- Velocity of central vertical and the horizontal planes through
- Two vel pipe axi
- The **jet**
- The **rec**
- Vertical of the v
- **Realiza** of the n towards
- Results location



RNG k-ε model  
303 mm



Realizable k-ε model

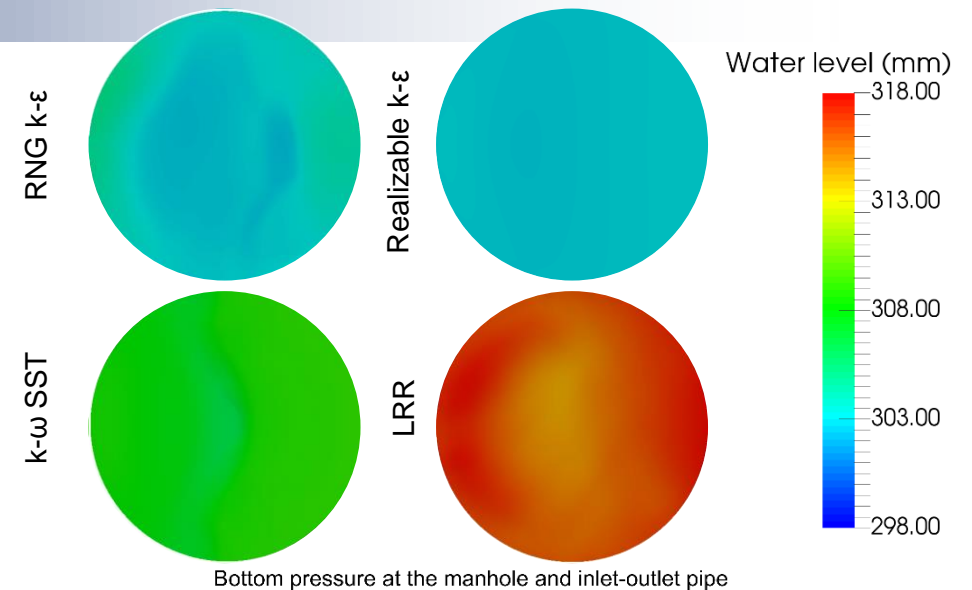


Velocity magnitude (m/s)

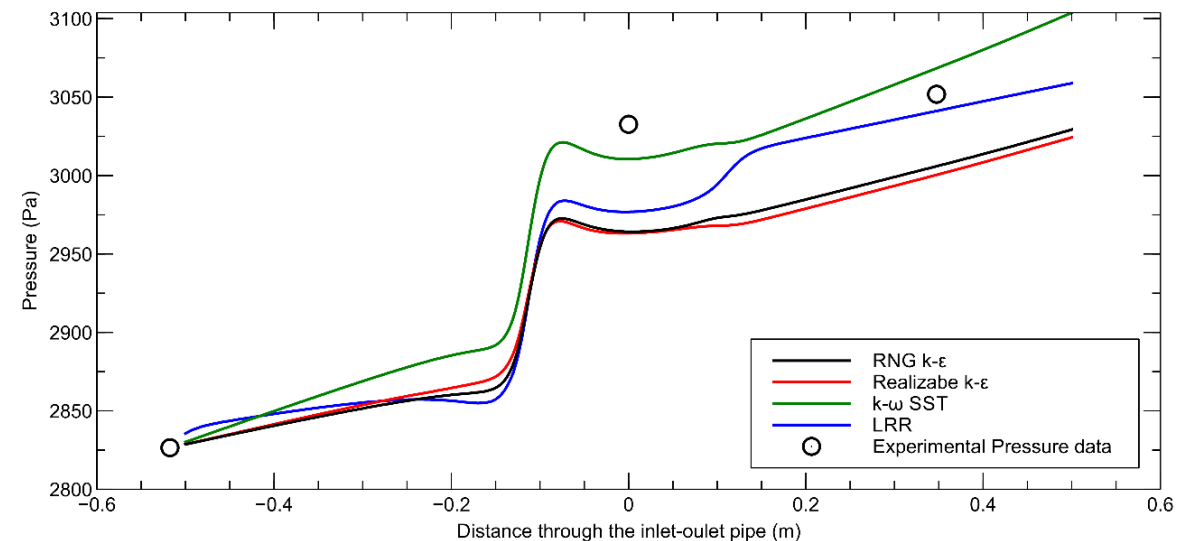


# Comparison between models

- Water depth was also found a little different at the manhole centre
  - RNG k- $\epsilon$ : 303mm
  - Realizable k- $\epsilon$ : 303mm
  - k- $\omega$  SST: 308 mm (Closest approximation)
  - LRR: 304mm
  - Experimental: 310mm

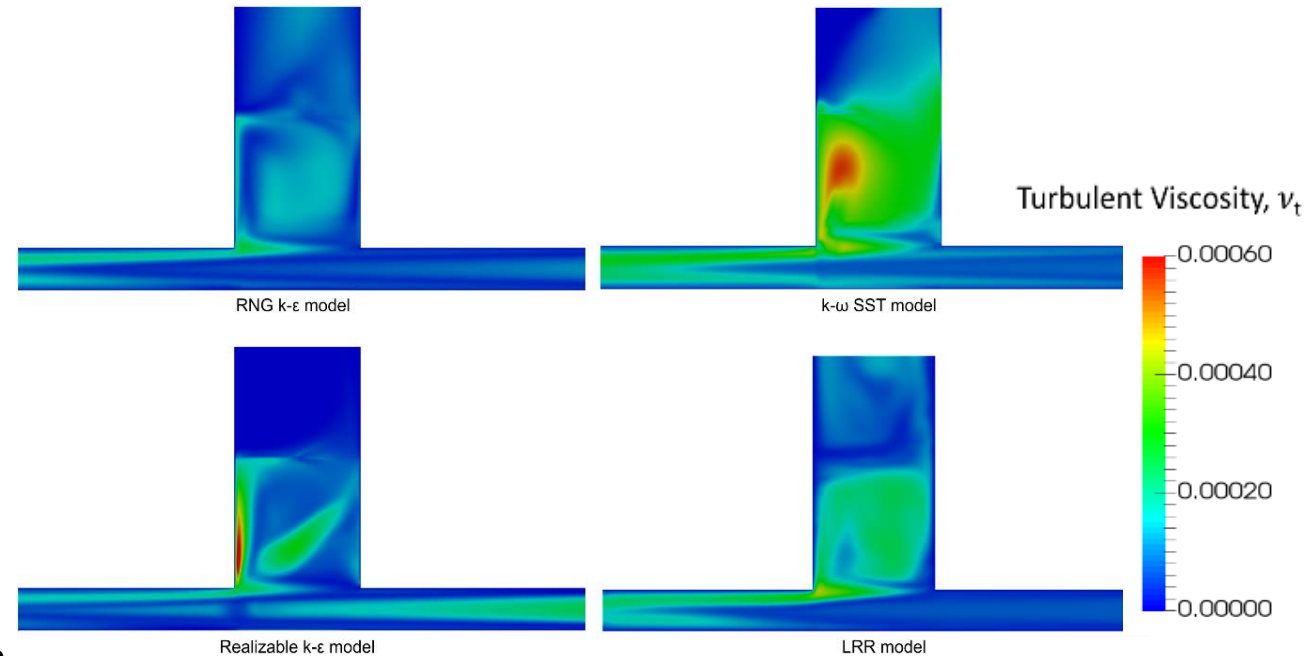


- The hydraulic grade line (HGL) of the manhole and throughout the length of inlet-outlet pipe is slightly different
  - RNG k- $\epsilon$  and Realizable k- $\epsilon$  models produce a similar pattern
  - No model could represent the same pressure pattern (few mm's different)



# Comparison between models

- RNG k-ε model showed the lowest turbulent viscosity ( $\nu_t$ )
- Realizable k-ε model showed very high  $\nu_t$  at the mid-section of the inlet pipe



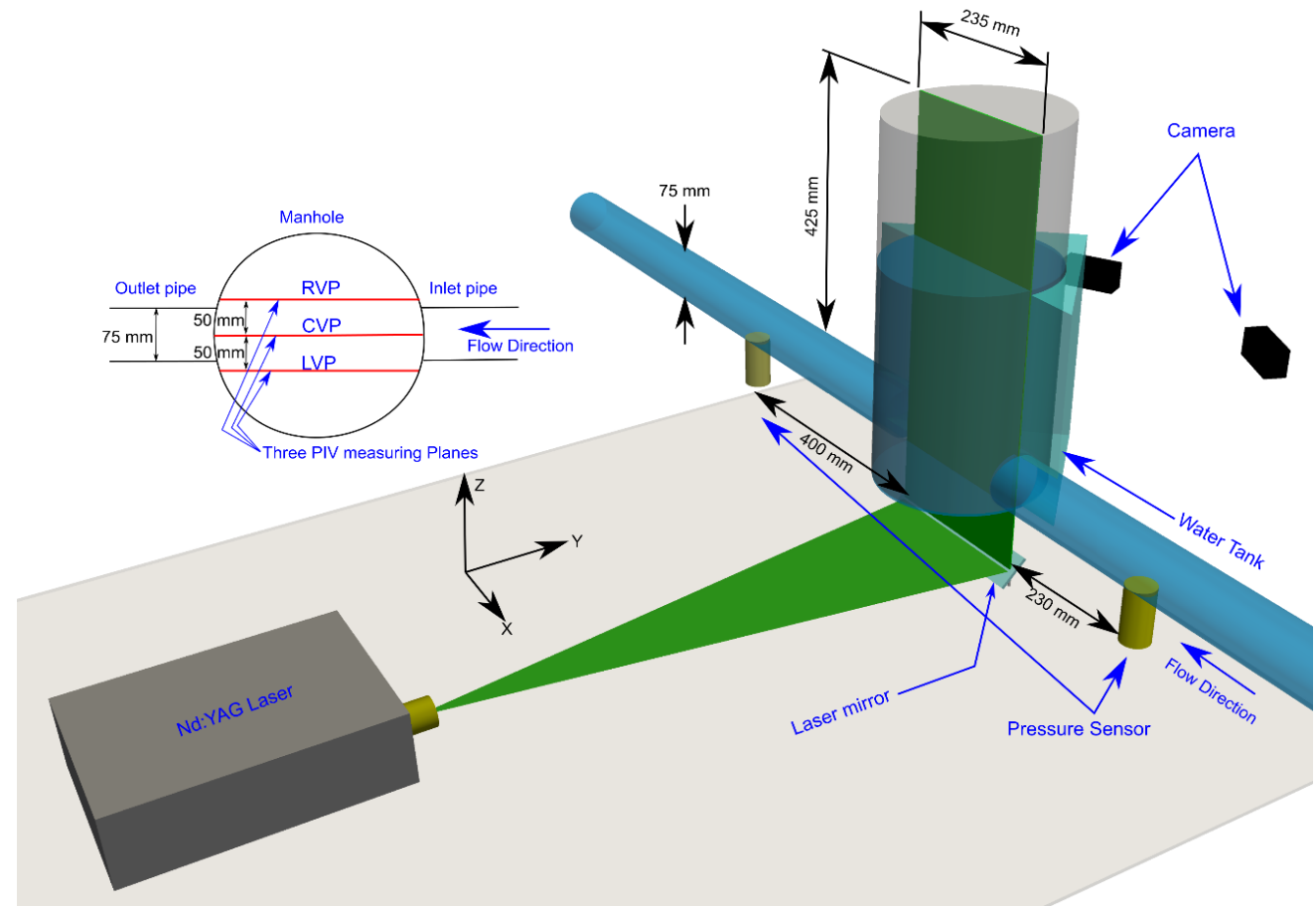
- The coefficient of head loss ( $k$ ) in the manhole is calculated as the ratio between head loss and the velocity head

$$k = \Delta H / \left( \frac{v^2}{2g} \right)$$

Simulation	Pressure drop		
	$\Delta P$ (Pa)	$\Delta H$	$k (= \Delta H / (v^2/2g))$
RNG k-ε	67.3	0.0069	<b>0.171</b>
Realizable k-ε	55.1	0.0056	<b>0.140</b>
k-ω SST	61.6	0.0063	<b>0.156</b>
LRR	121.4	0.0140	<b>0.307</b>

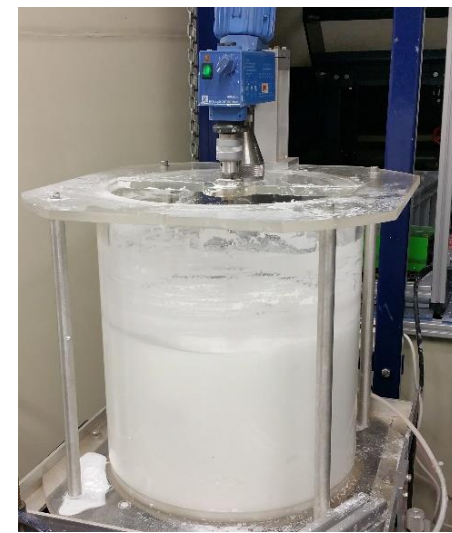
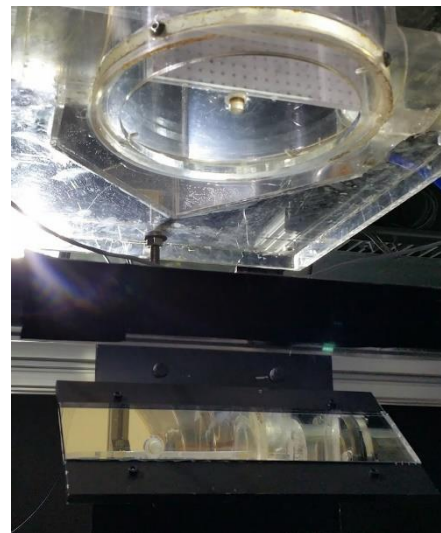
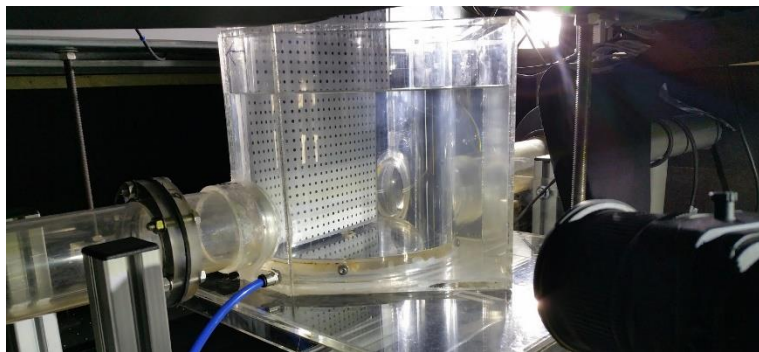
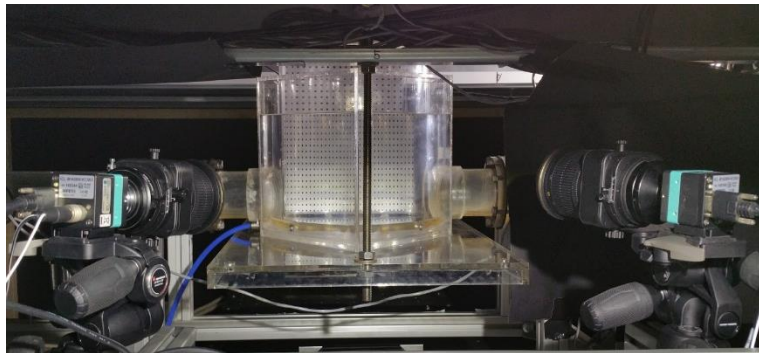
# Experimental Setup

- The experimental facility is installed at the hydraulic laboratory of University of Sheffield
- Transparent Perspex circular scaled manhole with inner diameter of **235 mm**
- Connected with a **75 mm** co-axial inlet-outlet pipe
- Pipe axis passes through the centre of the manhole axis.
- Two valves at the inlet and outlet that control the flow
- The inflow can be monitored using an electromagnetic flow meter.
- Two pressure sensors installed at the inlet and outlet pipes measure piezometric pressures





# PIV Setup

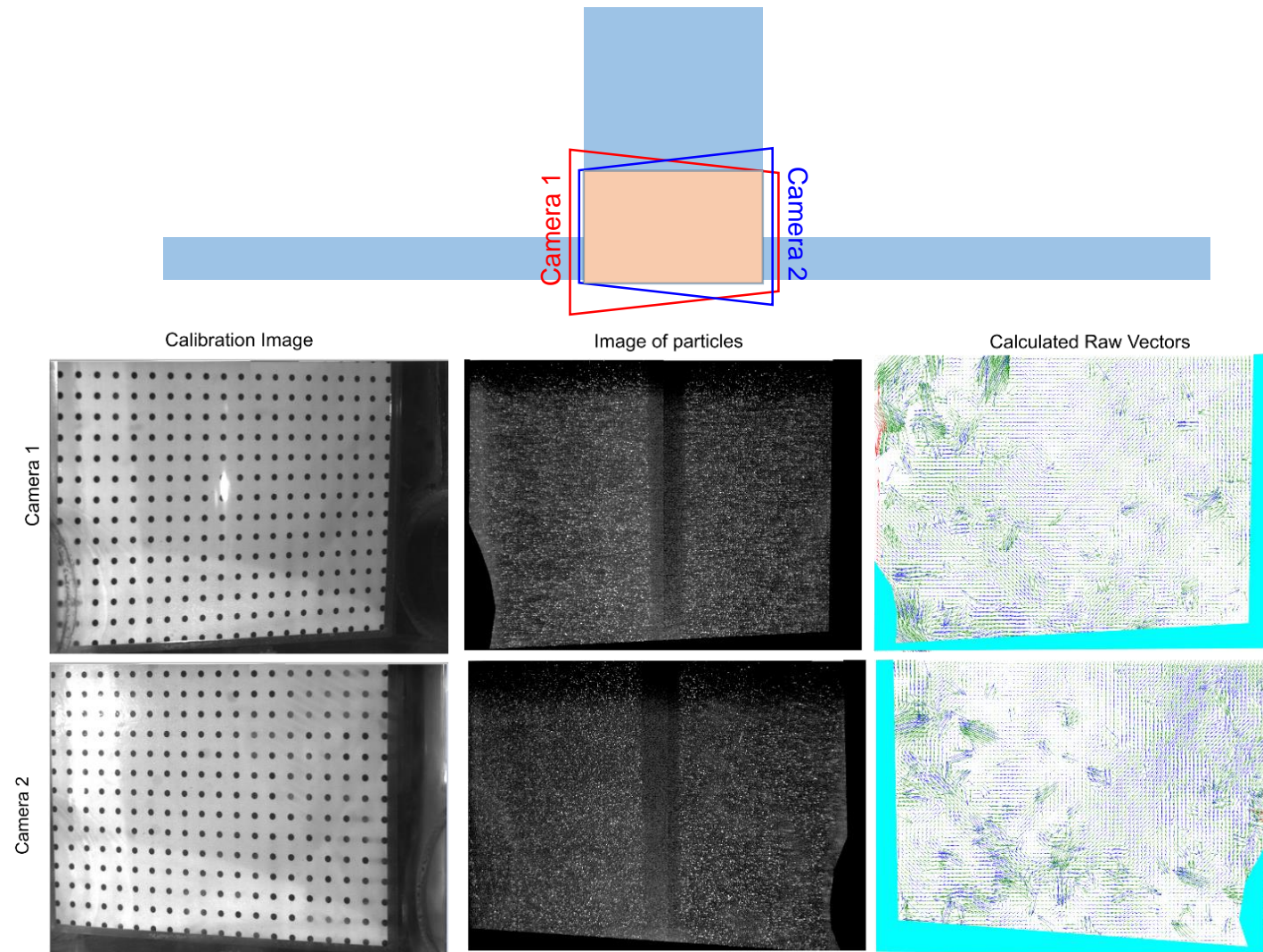


- Recently installed stereo PIV measurement consists of two Dantec FlowSense EO 2M cameras and a **Nd:YAG pulsed laser**
- Camera resolution is **1600x1200 pixels**
- Angle between the two cameras were more than  $45^\circ$
- To reduce error due to refraction at the curved manhole wall, a **transparent acrylic tank** was constructed around it and filled with water, keeping flat surfaces to both camera lenses.

- Laser was sent through the bottom of the manhole
- A laser mirror was used at  $45^\circ$  to the horizontal direction
- **100  $\mu\text{m}$  polyamide 12** particles were chosen for seeding

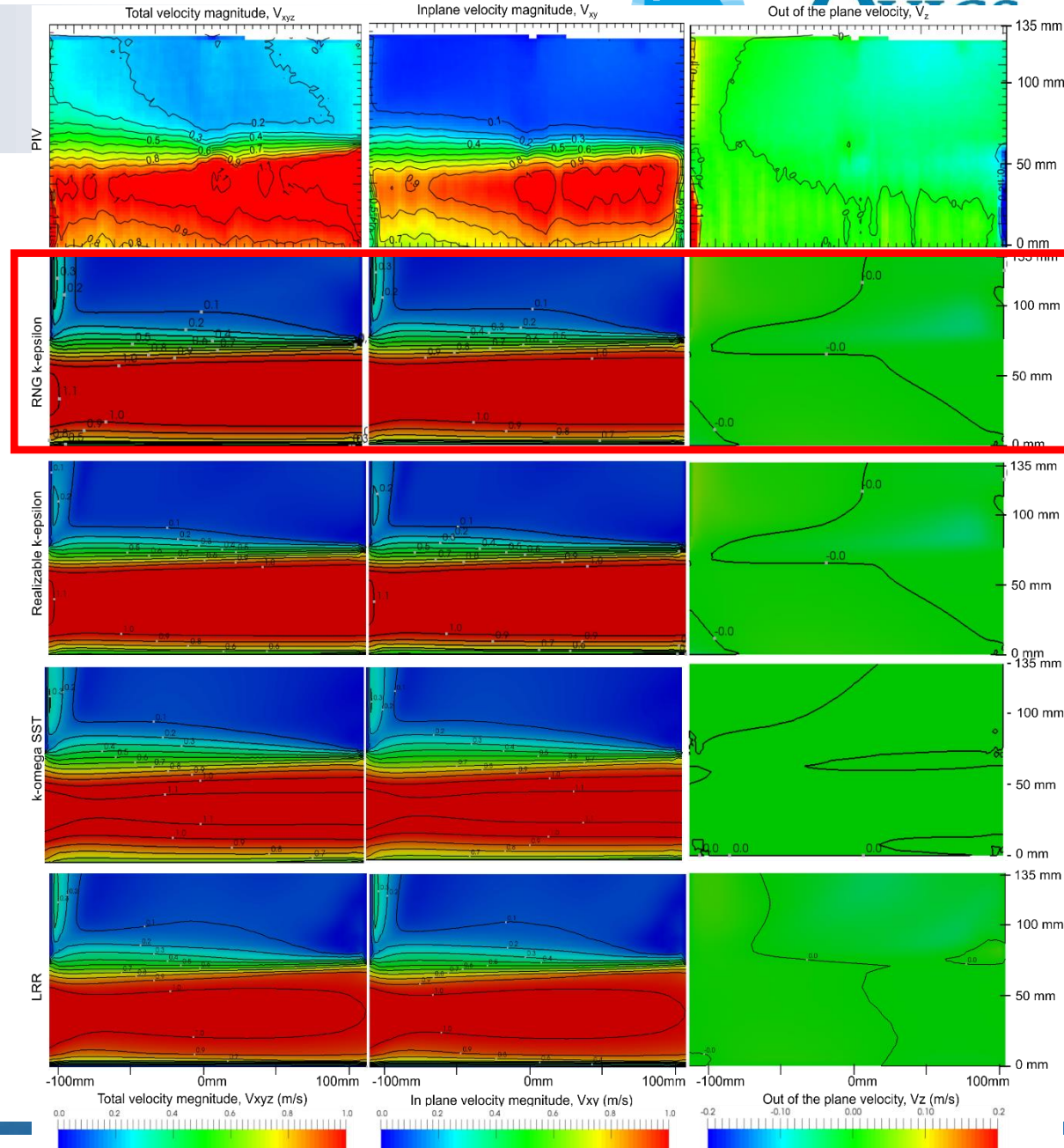
# PIV Measurement

- Data was taken using DynamicStudio v3.31
- Pre-processed using masking the area of interest
- Adaptive cross correlation technique was used to calculate the vectors
- Median correction post processing was applied to remove erroneous vectors.
- Neither of the cameras was able to cover the whole manhole height
- Only the core jet velocity zone was recorded



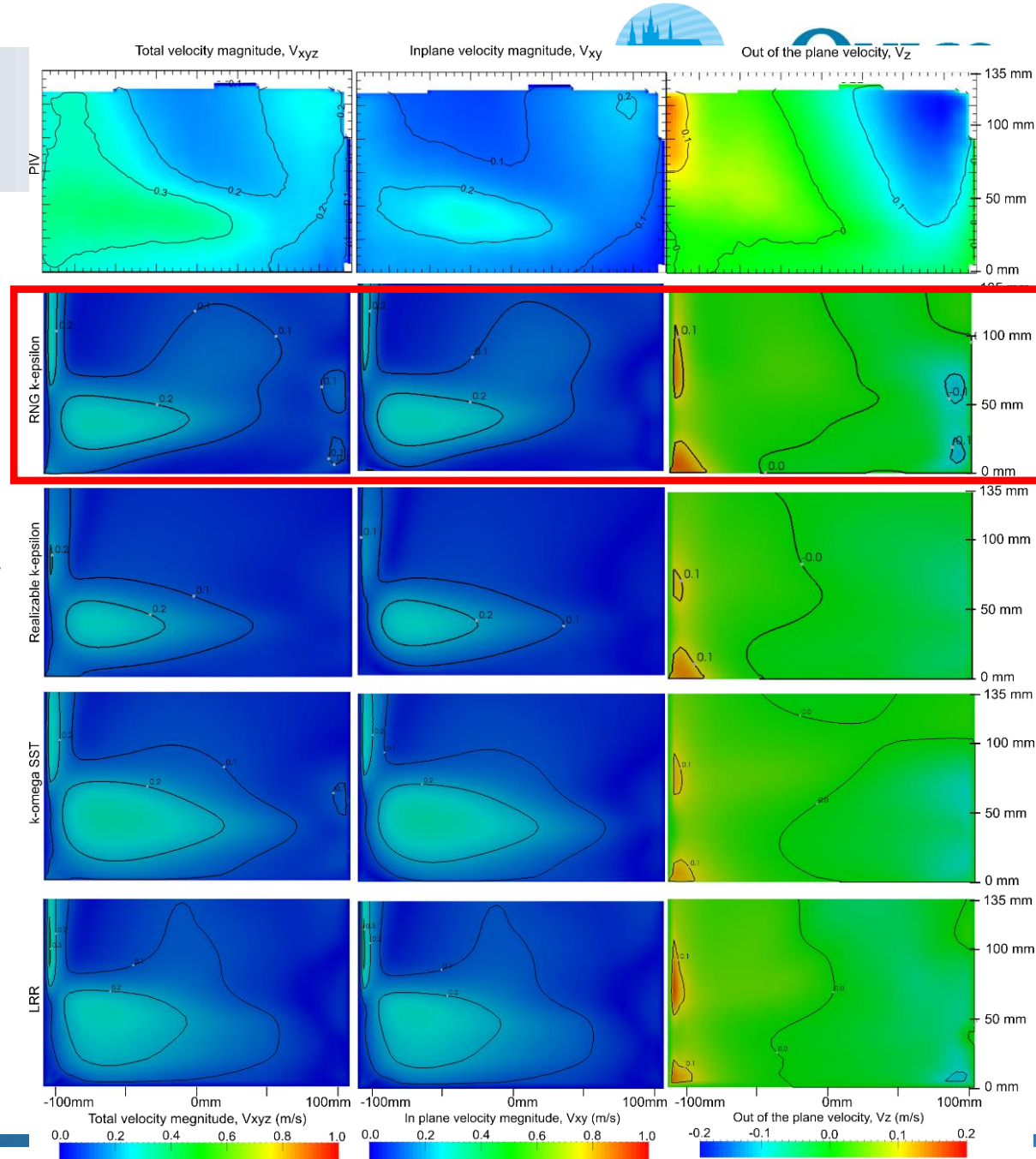
# Comparison with PIV

- PIV measurements were taken at the central vertical plane (CVP) along with the left vertical plane (LVP) and right vertical plane (RVP)
- At CVP, the core jet velocity zone in the RANS models were almost similar to PIV
- The diffusive velocity zone was also found similar
- CVP did not have much out of the plane velocity component ( $V_z$ )
- RNG k- $\epsilon$  and Realizable k- $\epsilon$  model show good match with PIV data at the CVP



# Comparison with PIV

- At LVP, The velocities measured through **PIV was found higher than CFD models**
- PIV measurement shows **higher the spread of the inlet jet velocity zone**
- At LVP, the highest jet velocity measured at PIV was up to 0.3 m/s and 0.2 m/s in CFD models
- The out of the plane velocity measurement ( $V_z$ ) at PIV is observed between -0.1 m/s to 0.2 m/s (Negative values  $V_z$  means direction towards the camera and positive value represents away from the camera)
- Similar  $V_z$  near the outlet of the manhole shown by numerical models
- **RNG k- $\epsilon$  model creates the closest approximation of the velocity at the manhole.**



# Conclusions

- A **scaled inline manhole to pipe diameter ratio** was **3.13** was studied
- Numerical simulations using **CFD with four different RANS** models
- Two dimensional plane with **three component (2D3C) stereo PIV measurement**
- Each model calculates the **velocity inside manhole** slightly differently
- Numerical models calculated marginally lower velocities towards all the three directions in compared to the PIV data
- Velocity structures and locations of vortex centres were found marginally different among the models
- The **RNG k- $\epsilon$  model** showed the **closest approximation of velocity contour** while **k- $\omega$  SST model** showed the **closest approximation of the water and pressure level** at the manhole

# Acknowledgement



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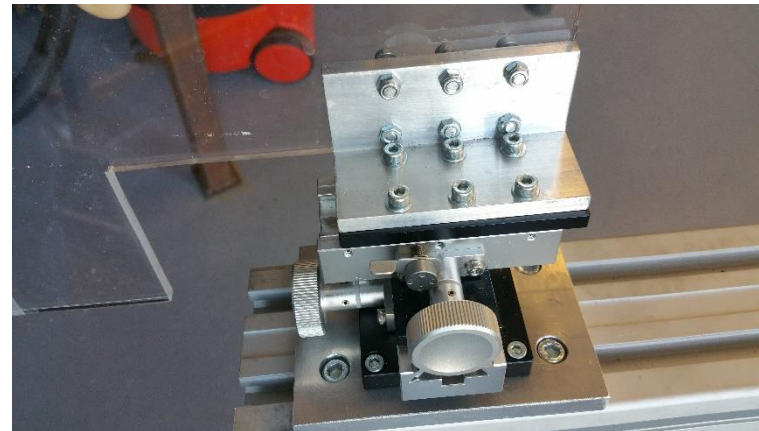
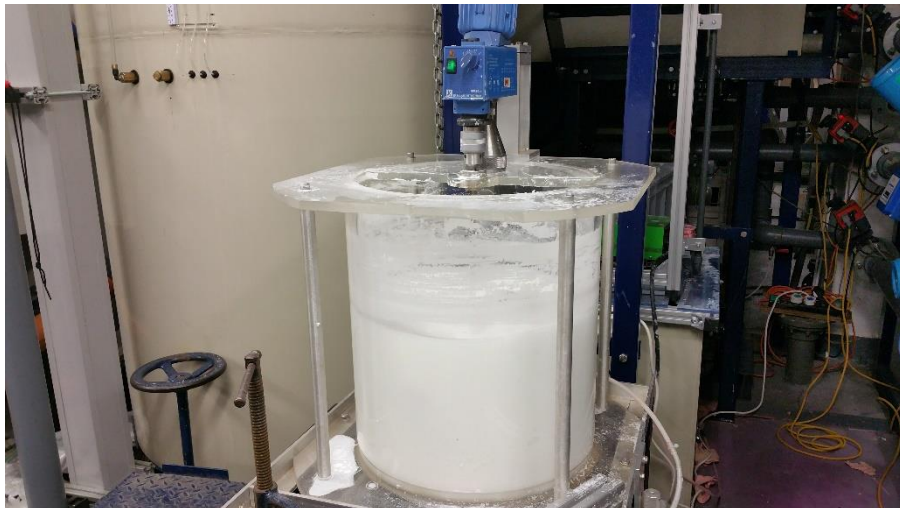
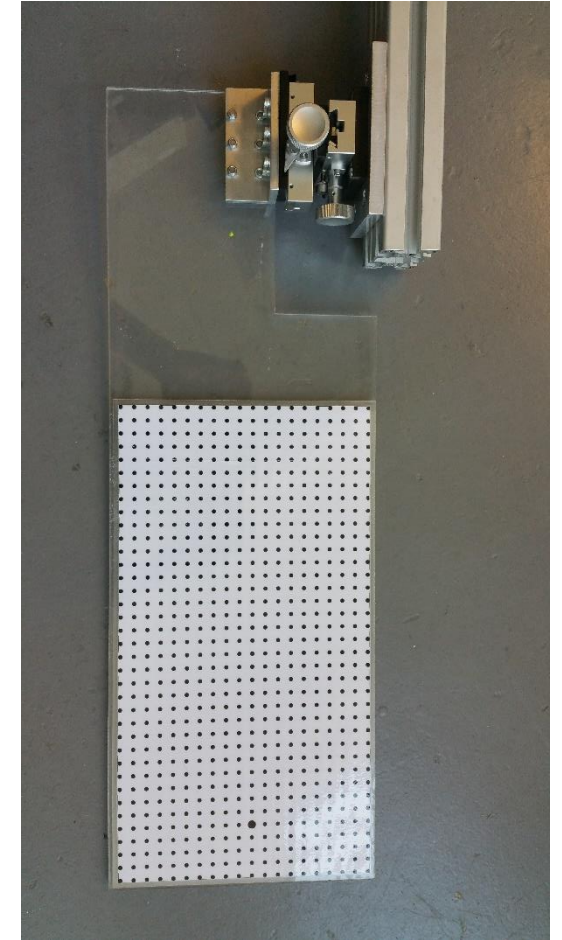
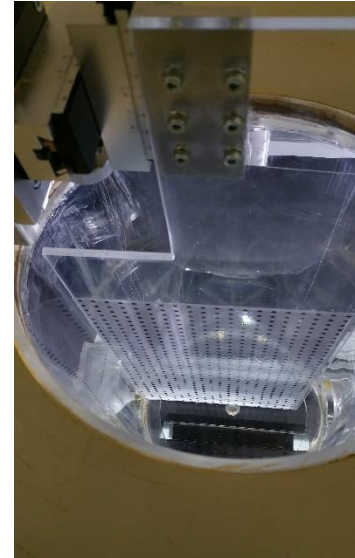
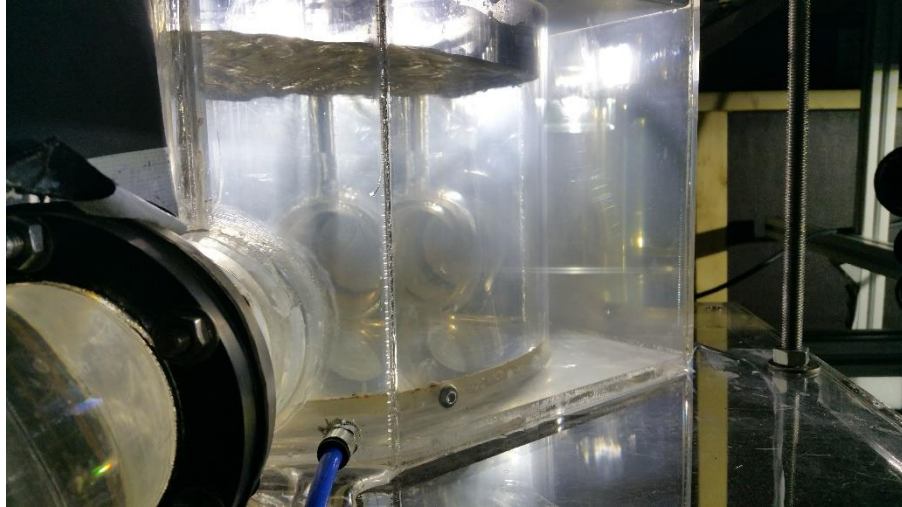
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# Thanks for your attention!



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# Experimental Setup





# Comparison between models

